

Original Research Paper

# Extraction Optimization of Essential Oil from *Medicago hispida* and Preliminary Inhibitory Mechanism Against *Escherichia coli*

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## Article history

Received: 12-08-2021

Revised: 10-11-2021

Accepted: 03-11-2021

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**Abstract:** In this study, the extraction optimization, characterization, antioxidant evaluation and preliminary inhibitory mechanism against *Escherichia coli* of the essential oil from dried *Medicago hispida* (EOMH) were explored to uncover the pending questions that had been raised in our previous work and to enlarge the industrial potential of EOMH production. The optimal parameters for EOMH extraction were: Extraction time of 7 h, particle size of 20 mesh and liquid-to-solid ratio of 30: 1 (mL/g), under which the highest yield of EOMH reached 0.31%. Nineteen constituents were identified in EOMH by gas chromatography mass spectrometry analysis, among which phytol content was up to 53.6%. These structures were further confirmed by infrared spectroscopy analysis. EOMH exerted similar scavenging capacities against Diphenyl Picryl Hydrazinyl (DPPH) and hydroxyl radicals with those of phytol. However, EOMH elicited stronger inhibitory effect on *E. coli* than that of phytol via shrinking *E. coli* cells, indicating that other factors, in addition to the antioxidant mechanism would equally affect the inhibitory effect of EOMH against *E. coli*, which should be deepened in the near future. In summary, present work would provide evidence for the industrial production and application of EOMH.

**Keywords:** *Medicago hispida*, Essential oil, Extraction Optimization, Phytol, Antioxidation, Inhibition on *E. coli*

## Introduction

Essential Oils (EOs) of plants are volatile aromatic substances extracted and refined from flowers, leaves, roots, seeds or fruits and are existed mostly as colorless or pale yellow oily viscous liquids at room temperature (Mirza and Navaei, 2009). EOs are almost insoluble in water, but are highly soluble in low-polarity organic solvents, including ether and petroleum ether. Meanwhile, EOs are complex mixtures composed of diverse compounds. Generally, one type of EOs contains tens to hundreds of components (Mirza and Navaei, 2009). According to chemical structures, EOs can be divided into four types, including terpenes, aromatics, aliphatics and sulfur/nitrogen-containing compounds. Special compositions endow the EOs with various bioactivities (Huang *et al.*, 2012; Wang *et al.*, 2017), such as antioxidant, antibacterial and antiviral activities. So far, the methods for EOs extraction are focused on steam distillation (Cassel *et al.*, 2009), organic solvent extraction, ultrasonic wave and/or microwave-assisted extractions (Guo *et al.*, 2012). Although advanced auxiliary extraction techniques exhibit certain advantages on increasing extraction yield, traditional steam distillation is

still the most frequently considered method for EOs extraction due to low cost and easier operation.

Current researches on genus *Medicago* are concentrated on *Medicago sativa*. For instance, comprehensively evaluated the quality of *M. sativa* using near-infrared spectroscopy (Wang *et al.*, 2016). Studied the bioactivities of *M. sativa* (Liu *et al.*, 2018). Other researchers (Krakowska *et al.*, 2017) were focused on the structure-activity relationships of active substances extracted and purified from *M. sativa*. In summary, *M. sativa* is the species belonging to *Medicago* family that has been received comprehensively studied and the substances of interest are polysaccharides, flavonoids and saponins. However, there is less research or exploitation on *Medicago hispida*, another common species of *Medicago*. In China, *M. hispida* is usually consumed as delicious vegetable and it contains many nutrients such as carbohydrates, proteins, vitamins and trace elements. The medicinal use of *M. hispida* was first described in Mingyi Bielu in the Han dynasty. Modern pharmacological investigations confirmed the hypoglycemic effects of total saponins from *M. hispida* and the antibacterial and antioxidant activities of total flavonoids from *M. hispida* (Cheng *et al.*, 2016). Nevertheless, there is little information

on the EOs from *M. hispida*. In previous work (Zheng *et al.*, 2019), we extracted the essential oil from fresh *M. hispida* (EOFMH) by using stem distillation and analyzed the chemical components with gas Chromatography-Mass Spectrometry (GC-MS). At the same time, we found that EOFMH exerts significant inhibitory activity against *E. coli*, which is similar to that of Chloromycetin, a chemically obtained antibacterial drug and EOFMH is dominated by phytol, accounting for 48.8% of the total content of EOs in EOFMH. Thus we conjectured that the promising inhibitory activity against *E. coli* of EOFMH would be mainly contributed by the abundant phytol and the bacteriostatic activity would be partially related to the antioxidant potential contributed by phytol. However, these hypothesizes are urgently needed to be confirmed by further experimental studies.

In the present investigation, considering the promising inhibitory activity against *E. coli*, firstly, we further optimized the steam distillation process of essential oil from *M. hispida* (EOMH) via Response Surface Methodology (RSM) coupled with Box-Behnken Design (BBD) involving liquid-solid ratio, extraction time and particle size as single factors. Meanwhile, due to the fact that dried raw material is easier to be preserved, especially for continuous industrial production, in this study, dried *M. hispida* was selected as raw and processed materials instead of fresh ones. Secondly, GC-MS and Fourier Transform Infrared spectroscopy (FT-IR) were used to identify and confirm the chemical profile of obtained EOMH. Thirdly, the *in vitro* antioxidant capacities of EOMH were tested. Finally, the preliminary mechanism of EOMH against *E. coli* was uncovered by Scanning Electron Microscopy (SEM). This continuous work is more likely to expand and validate our previous work (Zheng *et al.*, 2019) and to underlie the further researches on EOMH theoretically.

## Materials and Methods

### Materials and Chemicals

*M. hispida* materials used in this study were collected at the farmland of Southeast Development Zone, Changshu, Jiangsu, China on November 11, 2020 and were authenticated by Prof. Jianhua Hao, Changshu Institute of Technology, Changshu, Jiangsu, China. All the reagents and chemicals were analytically pure and microbial strain was stored at School of Biology and Food Engineering, Changshu Institute of Technology, Changshu, Jiangsu, China.

### Essential Oil Extraction

Fresh and cleaned *M. hispida* were dried at 60°C in an electric blast drying oven, crushed and sieved into different particle sizes. At each time, an appropriate amount of the crushed samples was put into a 2000 mL flask and then added certain water for soaking overnight. The flask was

connected to a steam distilling apparatus for certain time of reflux extraction at 105°C. After heating and cooling down, the liquids at the bottom of the flask were filtered out and the upper yellow oil was the obtained *Essential oil* from *M. hispida* (EOMH), which was collected and reserved in a collecting tube for further analysis (Cui *et al.*, 2018).

The essential oil extraction rate  $Q$  (%) was calculated as follows:

$$Q = \frac{m}{M} \times 100\% \quad (1)$$

Where:

$m$ : Mass of essential oil, g

$M$ : Mass of dried *M. hispida*, g

### Single-Factor Tests

Single-factor tests involving three factors (extraction time, particle size, liquid-to-solid ratio) were conducted. The effects of different factors on EOMH extraction rate were studied. The three factors were set as follows: extraction time (3 ~ 11 h), particle size (0 ~ 40 mesh) and liquid-to-solid ratio (10: 1 ~ 50: 1 mL/g) (Cui *et al.*, 2018).

### Response Surface Methodology (RSM) Optimization

According to the results of single-factor tests, the effects of process parameters on EOMH extraction rate were optimized by RSM coupled with Box-Behnken Design (BBD). The effects of different factors, either alone or in combination on EOMH extraction rate were compared to optimize the EOMH extraction. The factor levels and codes of BBD were listed in Table 1.

The experimental data were analyzed by multifactor fitting regression on Design-Expert 8.0.6.1. Then a two-order polynomial model in the form of equations was built:

$$Y = \beta_0 + \sum_{i=1}^n \beta_i X_i + \sum_{i=1}^n \beta_{ii} X_i^2 + \sum_{i < j}^n \beta_{ij} X_i X_j + \varepsilon \quad (2)$$

Where:

- $Y$  = The predicted extraction rate of EOMH
- $\beta_0$  = A constant coefficient
- $\beta_i, \beta_{ii}$  and  $\beta_{ij}$  = First-order quadratic coefficients of  $X_i$
- $\varepsilon$  = The experimental error

**Table1:** The factor levels and codes used in the RSM

	Level		
	-1	0	1
$X_1$ : Extraction time (h)	5	7	9
$X_2$ : Particle size (mesh)	10	20	30
$X_3$ : Liquid-to-solid ratio (mL/g)	20: 1	30: 1	40: 1

### GC-MS Analysis

Chemical constituents of EOMH were analyzed by a QP-2010 gas chromatography mass spectrometry (GC-MS) (Shimadzu, Kyoto, Japan) installed with a Rxi-5Sil MS column (30 m × 0.25 mm × 0.25 μm). The analytical processes were as follows: Helium was served as carrier gas with flow rate of 1.0 mL/min; the initial column temperature was set to 40°C (maintained for 4 min), then reached to 60°C (heating rate of 5°C/min, maintained 2 min at 60°C), raised from 60°C to 110°C at 15°C/min (maintained 4 min at 110°C), then raised from 110°C to 180°C at 5°C/min (maintained 5 min at 180°C), finally climbed to 280°C at 25°C/min (maintained 5 min at 280°C); ion trap temperature was 230°C; transmission line temperature was 250°C; scan range was from 35 to 500 amu and ionization energy was 70 eV. One microliter of EOMH was dissolved in ether to a total concentration of 12 mg/mL and injected into the column at a split ratio of 1: 30. Constituents in EOMH were authenticated though comparing both the Retention Index (RI) relative to the mass spectra library (NIST 05) (Elkady and Ayoub, 2018) and the standards of C<sub>8</sub>-C<sub>40</sub> *n*-alkanes.

### FT-IR Analysis

Based on a method from Boughendjioua *et al.* (2020), EOMH and phytol standard were characterized by FT-IR. At each time, 50 μL of sample was dripped on a glass slide, which was gently shaken to make the sample distribute evenly to form a thin layer. After acquisition of background information, the sample was scanned by using a Fourier transform infrared spectrometer from 4000 to 400 cm<sup>-1</sup>.

### The In Vitro Antioxidant Activities

#### DPPH Radical Scavenging Capability

The method from Javad *et al.* 2009 was adopted with minor modifications. EOMH and phytol standard were both dissolved in dimethyl sulfoxide to produce the final concentrations of 0.2, 0.4, 0.6, 0.8, 1.0, 1.2 mg/mL. Each sample (2 mL) was sucked into a test tube and mixed with 1 mL of 0.1 mmol/L DPPH solution, which was tested sample. The control sample was prepared by using anhydrous ethanol instead of the DPPH solution. The blank sample was prepared by using anhydrous ethanol instead of tested sample. The three groups of samples were completely oscillated and evenly mixed, followed by being placed in the dark for 30 min. After that, the absorbance at 517 nm of each sample was detected. Vitamin C (Vc) was used as positive control, each test was repeated for three times. DPPH radical scavenging rate was calculated as follows:

$$\text{DPPH radical scavenging rate (\%)} = \left(1 - \frac{A_i - A_j}{A_0}\right) \times 100 \quad (3)$$

Where:

A<sub>0</sub>: Absorbance of the blank  
A<sub>i</sub>: Absorbance of the sample  
A<sub>j</sub>: Absorbance of the control

#### Hydroxyl Radical Scavenging Capability

The method from Chen *et al.*, 2007 was referenced with minor modifications. EOMH and phytol standard were dissolved in dimethyl sulfoxide to give the final concentrations of 0.2, 0.4, 0.6, 0.8, 1.0, 1.2 mg/mL, respectively. Each sample (1 mL) was sucked into a test tube and mixed with 1 mL of 6 mmol/L FeSO<sub>4</sub> solution and 1 mL of 6 mmol/L H<sub>2</sub>O<sub>2</sub> solution. The sample was evenly shaken and placed at room temperature for 10 min. Then 1 mL of 6 mmol/L salicylic acid solution was added. The blank sample was prepared by replacing tested sample with distilled water. The control sample was obtained by substituting distilled water for salicylic acid solution. The three groups of samples were fully shaken and placed in water bath at 37°C for 0.5 h. After that, the absorbance at 510 nm was detected. Vc was served as positive control. Each sample was tested in triplicate. The hydroxyl radical scavenging rate was computed as follows:

$$\text{Hydroxyl radical scavenging rate (\%)} = \left(1 - \frac{A_i - A_j}{A_0}\right) \times 100 \quad (4)$$

Where:

A<sub>0</sub>: Absorbance of the blank  
A<sub>i</sub>: Absorbance of the sample  
A<sub>j</sub>: Absorbance of the control

#### Preliminary Inhibitory Mechanism against *E. coli*

The morphological changes of *E. coli* were scanned by SEM (Zhan *et al.*, 2014a). Three groups were set as follows: One group was treated with EOMH, another group was dealt with phytol and one was the activated *E. coli* suspension (600 nm, OD: 0.5) (blank control). EOMH and phytol standard were dissolved in dimethyl sulfoxide, respectively. All samples (20 μL of each) were fully mixed with 180 μL of above-mentioned suspension, forming the treated groups. Then 200 μL of suspension was used as the blank control. After cultivation in a thermostatic incubator at 37°C for 16 h, one drop from each sample was collected and put into a dissociated mica slide, which was metal-sprayed and observed under SEM.

#### Statistical Analysis

All the assays in this study were performed in triplicate and the results were presented as means or means ± standard error. The experimental data were statistically tested by analysis of one-way Analysis of Variance (ANOVA). *P*<0.05 was deemed as significant difference.

## Results

### Single-Factor Tests

#### Effects of Extraction Time, Particle Size and Liquid-to-Solid Ratio on Extraction Rate of EOMH

The effect of extraction time on EOMH extraction rate was illustrated in Fig. 1, which showed that the optimal extraction time was 7 h. As shown in Fig. 2, the extraction rate of EOMH was maximized when the particle size of dried *M. hispida* reached 20 mesh. The effect of liquid-to-solid ratio on EOMH extraction rate was illustrated in Fig. 3 and the extraction rate was maximized to 0.25% at the liquid-to-solid ratio of 30: 1 mL/g. The effects of above-mentioned three single factors on the extraction rate of EOMH all appeared an upward trend first and then a downward trend.

### RSM Optimization

The extraction rate of EOMH was optimized by RSM. Experimental data in Table 2 were fitted on Design-Expert software. A regression equation was established as follows:

$$Y = -1.33794 + 0.19538X_1 + 0.042275X_2 + 0.036475X_3 - 1.125 \times 10^{-3} X_1X_2 + 1.25 \times 10^{-4} X_1X_3 + 7.5 \times 10^{-5} X_2X_3 - 0.012438X_1^2 - 9.475 \times 10^{-4} X_2^2 - 6.475 \times 10^{-4} X_3^2 \quad (5)$$

The calibration coefficient was  $R^2 = 0.9823$  and the Coefficient of Variation (CV) was 6.58%. Simulation and fitting with regression equations showed that this experimental model can well reflect the relationships of different factors with EOMH extraction rate and could be

effective for simulating computation and thereby returning real experimental data.

The model was featured with  $P < 0.0001$  and error  $P = 0.3717$  (Table 3). Analysis of Variance (ANOVA) and tests proved that this model is highly significant and can yield accurate data. Results of ANOVA showed that among the single terms, the influence of particle size ( $X_2$ ) on EOMH yield surpasses those of extraction time ( $X_1$ ) and liquid-to-solid ratio ( $X_3$ ). The influence of between-factor interaction on extraction rate ranked as:  $X_1X_2 > X_2X_3 > X_1X_3$ . The effects of squares of each factor on the extraction rate ranked as:  $X_2^2 > X_3^2 > X_1^2$ .

During the extraction of EOMH, the contours and 3D RSM images illustrated the effects of between-factor interactions on the extraction rate (Fig. 4). As for the interaction between extraction time and particle size, the RSM images (Fig. 4b) were abrupt and the contours were ellipse-shaped (Fig. 4a). The interaction between extraction time and particle size significantly affected EOMH yield ( $P = 0.015$ ) (Huang *et al.*, 2013). As for the interaction between extraction time and liquid-to-solid ratio, the contours in Fig. 4c were shaped similarly as that in Fig. 4e, but the 3D RSM images were more circular. Hence, the influence of particle size on EOMH extraction slightly surpassed the influence of liquid-to-solid ratio. As for the interaction between liquid-to-solid ratio and particle size, the RSM images (Fig. 4f) were gentle and the contours (Fig. 4e) were nearly round-shaped. Therefore, the interaction between liquid-to-solid ratio and particle size did not significantly affect EOMH extraction rate ( $P = 0.3208$ ). The results from the contours and 3D RSM images were generally consistent with the results presented in Table 3.

**Table 2:** Box-Behnken design and experimental data

Run	Independent variable			Extraction rate (%)	
	$X_1$	$X_2$	$X_3$	Actual value	Predicted value
1	-1	-1	0	0.15	0.15
2	1	-1	0	0.22	0.21
3	-1	1	0	0.16	0.17
4	1	1	0	0.14	0.14
5	-1	0	-1	0.20	0.20
6	1	0	-1	0.19	0.20
7	-1	0	1	0.20	0.19
8	1	0	1	0.20	0.21
9	0	-1	-1	0.17	0.17
10	0	1	-1	0.14	0.13
11	0	-1	1	0.15	0.16
12	0	1	1	0.15	0.15
13	0	0	0	0.32	0.31
14	0	0	0	0.31	0.31
15	0	0	0	0.30	0.31
16	0	0	0	0.33	0.31
17	0	0	0	0.30	0.31

$X_1$ : Extraction time (h)

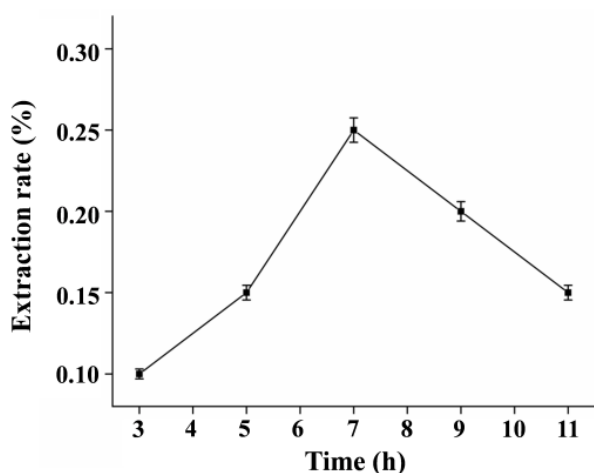
$X_2$ : Particle size (mesh);

$X_3$ : Liquid-to-solid ratio (mL/g)

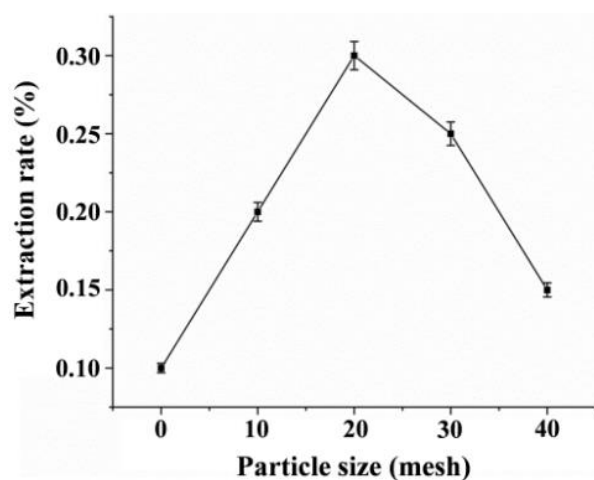
**Table 3:** Analysis of variance

Source	Df	Sum of squares	Mean square	F-value	P-value	Significance <sup>a</sup>
Model	9	0.077	$8.512 \times 10^{-3}$	43.18	<0.0001	**
$X_1$	1	$2.000 \times 10^{-4}$	$2.000 \times 10^{-4}$	1.01	0.3474	n.s.
$X_2$	1	$1.250 \times 10^{-3}$	$1.250 \times 10^{-3}$	6.34	0.0399	*
$X_3$	1	0.000	0.000	0.000	1.0000	n.s.
$X_1X_2$	1	$2.025 \times 10^{-3}$	$2.025 \times 10^{-3}$	10.27	0.0150	*
$X_1X_3$	1	$2.500 \times 10^{-5}$	$2.500 \times 10^{-5}$	0.13	0.7323	n.s.
$X_2X_3$	1	$2.250 \times 10^{-4}$	$2.250 \times 10^{-4}$	1.14	0.3208	n.s.
$X_1^2$	1	0.010	0.010	52.86	0.0002	**
$X_2^2$	1	0.038	0.038	191.74	<0.0001	**
$X_3^2$	1	0.018	0.018	89.54	<0.0001	**
Residual	7	$1.380 \times 10^{-3}$	$1.971 \times 10^{-4}$			
Lack of fit	3	$7.000 \times 10^{-4}$	$2.333 \times 10^{-4}$	1.37	0.3717	n.s.
Pure error	4	$6.800 \times 10^{-4}$	$1.700 \times 10^{-4}$			
Cortotal	16	0.078				

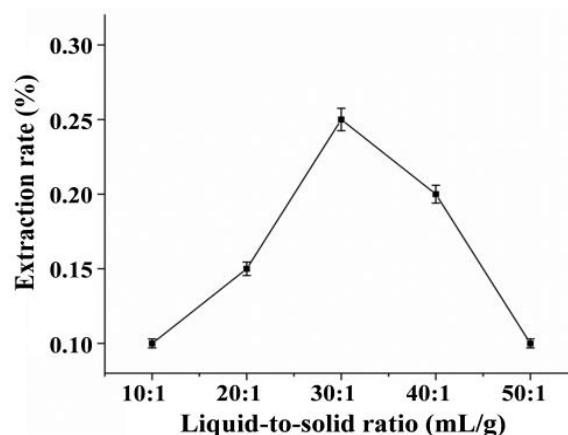
<sup>a</sup>\* $P < 0.05$  significant ; \*\* $P < 0.01$  highly significant ;  $P > 0.05$  not significant (n.s.); Lack of fit means the model is significant



**Fig. 1:** The effects of extraction time on the extraction rate of EOMH. Data was shown as means  $\pm$  SD (n = 3)



**Fig. 2:** The effects of particle size on the extraction rate of EOMH. Data was shown as means  $\pm$  SD (n = 3)



**Fig. 3:** The effects of liquid-to-solid ratio on the extraction rate of EOMH. Data was shown as means  $\pm$  SD (n = 3)

#### Verification of Optimal Process Parameters

Based on the RSM model, the optimal process for EOMH extraction was: Extraction time of 7.28 h, particle size of 18.49 mesh and liquid-to-solid ratio of 29.94: 1 (mL/g). To facilitate the practical operation, we adjusted the optimal process into extraction time of 7 h, particle size of 20 mesh and liquid-to-solid ratio of 30: 1 (mL/g). The average extraction rate from three parallel experiments was 0.31%, which was close to the predicted value, indicating that the obtained model is feasible for predicting the optimization of EOMH extraction.

#### GC-MS Profile

Nineteen constituents were identified in EOMH by GC-MS and results were presented in Table 4. These components were identical with the essential oil extracted from fresh *M. hispida*, but the content of each compound was different (Zheng *et al.*, 2019). Compared with EOFMH,

there were eight compounds missing in EOMH, the content of phytol in EOMH was raised to 53.6%, which was 9.84% higher than that in EOFMH.

#### FT-IR Analysis

The chemical profile of EOMH was further confirmed by FT-IR using phytol as control. From Fig. 5, it can be seen that the chemical structure of phytol contains special groups, including one carbon-carbon double bond (C = C) and one hydroxyl group (O-H). The FT-IR spectrum of EOMH showed peaks at 3433  $\text{cm}^{-1}$  (stretching vibration of O-H) and 1644  $\text{cm}^{-1}$  (stretching vibration of C = C). These peaks were similar to the stretching vibration peaks of standard phytol at 3373  $\text{cm}^{-1}$  (O-H) and 1659  $\text{cm}^{-1}$  (C = C). The result of FT-IR analysis was highly consistent with that of GC-MS determination (Table 4).

#### In Vitro Antioxidant Activity

##### DPPH Radical-Scavenging Capacity

Within the concentration range of 0.2 mg/mL ~ 1.2 mg/mL, EOMH can scavenge DPPH<sup>•</sup> to some extent (Fig. 6a). When the concentration gradually increased, the scavenging capability of EOMH against DPPH<sup>•</sup> was generally improved. At the concentration of 1.2 mg/mL, the scavenging rate was up to 65.05%. The DPPH<sup>•</sup> scavenging capability of phytol changed in the similar way as that of EOMH. At the concentration of 1.2 mg/mL, the scavenging rate reached 70.05%. The half maximal inhibitory concentration (IC<sub>50</sub>) values of EOMH and phytol were 0.022 mg/mL and 0.036 mg/mL, respectively. In

comparison, the DPPH<sup>•</sup> scavenging capability of EOMH was much stronger than that of phytol, but the DPPH<sup>•</sup> scavenging abilities were generally weaker than that of Vc.

##### Hydroxyl Radical-Scavenging Capacity

The hydroxyl radical (<sup>•</sup>OH) scavenging rates of EOMH and phytol were calculated. Then a relationship between concentration and scavenging rate was established (Fig. 6b). Clearly, the <sup>•</sup>OH scavenging capabilities of phytol and EOMH were elevated with the increment of concentration within the range of 0.2 ~ 1.2 mg/mL. At the concentration of 1.2 mg/mL, the <sup>•</sup>OH scavenging rates of EOMH and phytol were 68.02% and 72.77%, respectively. The corresponding IC<sub>50</sub> values were 0.271 and 0.290 mg/mL, respectively, suggesting that the <sup>•</sup>OH scavenging capability of EOMH was little weaker than that of phytol and also weaker than that of Vc.

##### Preliminary Inhibitory Mechanism Against *E. coli*

The SEM images of untreated *E. coli* suspension showed that the thalli was morphologically smooth and even on the whole and was complete and plump, with smooth and uninjured surface (Fig. 7a). After addition of phytol (Fig. 7b), the cell morphology was not changed largely, but the cells shrunk to some extent and were less plentiful. After treatment with EOMH, the cell morphology was changed significantly. The cells shrunk on the whole and the surface was rough with numerous folds (Fig. 7c).

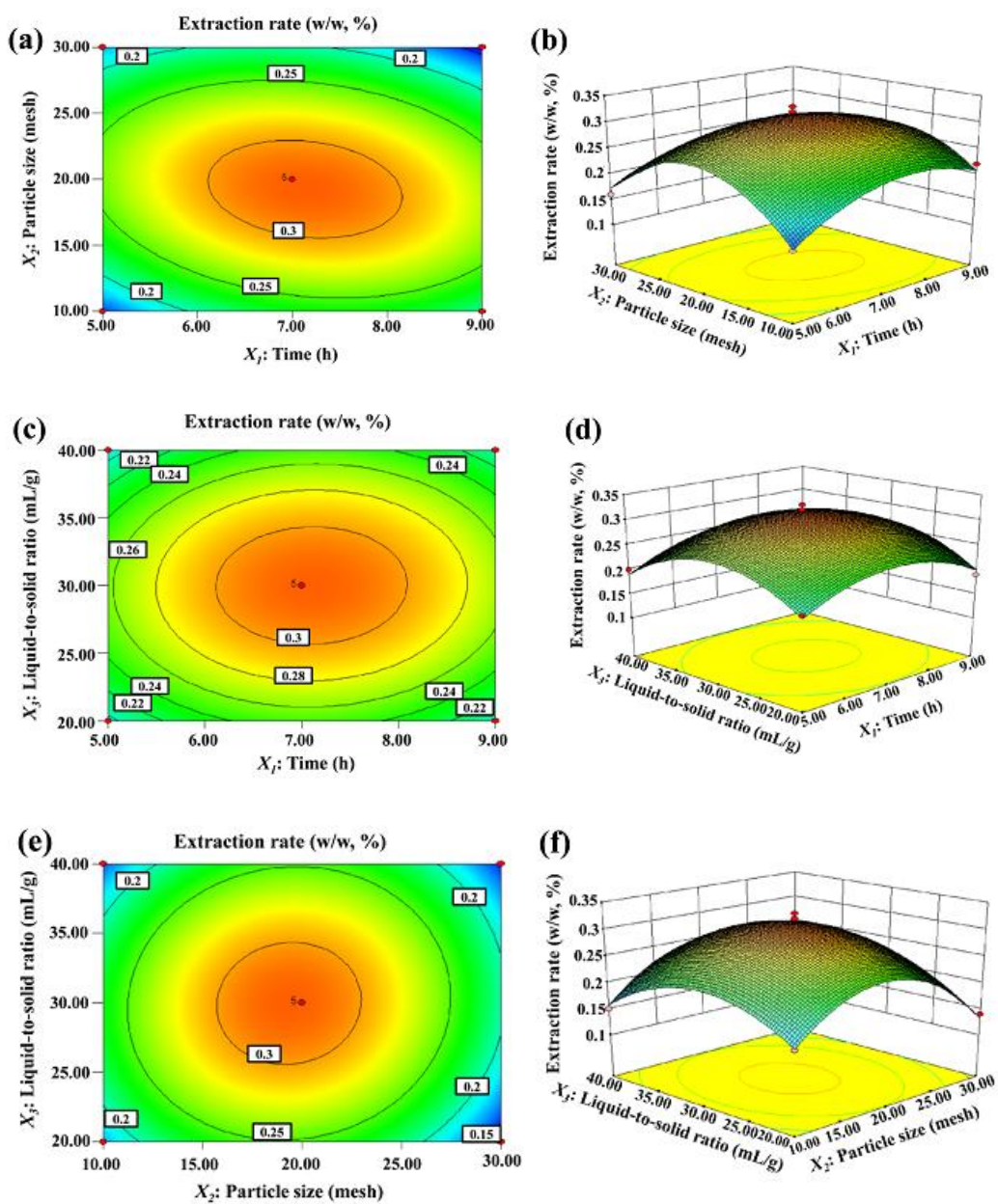
**Table 4:** Chemical profiles of EOMH

No.	Compounds	Molecular	RI	RI*	Type	%	
	formula	Rt/min					
1	Nonadecane	C <sub>19</sub> H <sub>44</sub>	35.28	1910	1910	Alkane	0.09
2	Eicosane	C <sub>20</sub> H <sub>42</sub>	37.79	2009	2002	Alkane	0.11
3	Ethyl heptadecanoate	C <sub>19</sub> H <sub>38</sub> O <sub>2</sub>	38.98	2077	2086	Ester	0.10
4	Elaidyl alcohol	C <sub>18</sub> H <sub>36</sub> O	39.28	2061	2119	Alcohol	0.13
5	Heneicosane	C <sub>21</sub> H <sub>44</sub>	39.42	2109	2138	Alkane	0.18
6	Docosane	C <sub>22</sub> H <sub>46</sub>	40.00	2208	2198	Alkane	2.81
7	Phytol	C <sub>20</sub> H <sub>40</sub> O	40.12	2200	2210	Alcohol	53.6
8	2-[[2-[(2-Ethylcyclopropyl)methyl]cyclopropyl]methyl]cyclopropanoic acid methyl ester	C <sub>22</sub> H <sub>38</sub> O <sub>2</sub>	40.45	2266	2262	Ester	0.38
9	Ethyl linolenate	C <sub>20</sub> H <sub>34</sub> O <sub>2</sub>	40.58	2201	2250	Ester	2.05
10	Cis-9-tricosene	C <sub>23</sub> H <sub>46</sub>	40.89	2315	2311	Alkene	3.39
11	Pentacosane	C <sub>25</sub> H <sub>52</sub>	42.25	2506	2508	Alkane	3.51
12	9-Hexacosene	C <sub>26</sub> H <sub>52</sub>	42.88	2614	2582	Alkene	2.12
13	Diisooctyl phthalate	C <sub>24</sub> H <sub>38</sub> O <sub>4</sub>	43.41	2704	2668	Ester	1.11
14	Hexacosane	C <sub>26</sub> H <sub>54</sub>	43.79	2606	2674	Alkane	5.09
15	1-Hexacosanol	C <sub>26</sub> H <sub>54</sub> O	44.51	2848	2780	Alcohol	3.28

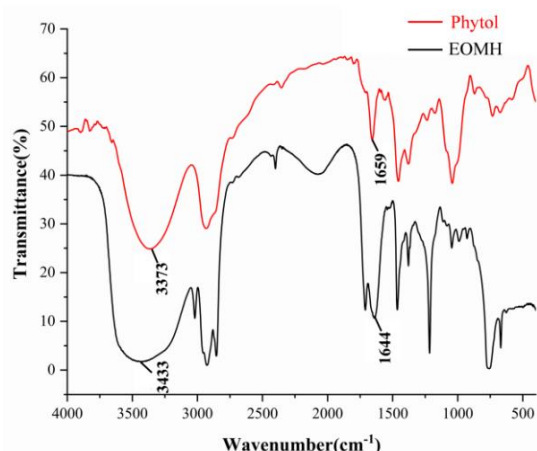
**Table 4:** Continue

16	Methyl pentacosanoate	C <sub>26</sub> H <sub>52</sub> O <sub>2</sub>	45.12	2773	2832	Ester	2.44
17	Nonacosane	C <sub>29</sub> H <sub>60</sub>	45.99	2904	2902	Alkane	4.10
18	Triacontane	C <sub>30</sub> H <sub>62</sub>	47.29	3003	2998	Alkane	6.46
19	Dotriacontane	C <sub>32</sub> H <sub>66</sub>	50.39	3202	3162	Alkane	4.31
	Total						95.3
	Diterpene alcohol compounds						53.6
	Alkane compounds						26.7
	Others						15.0

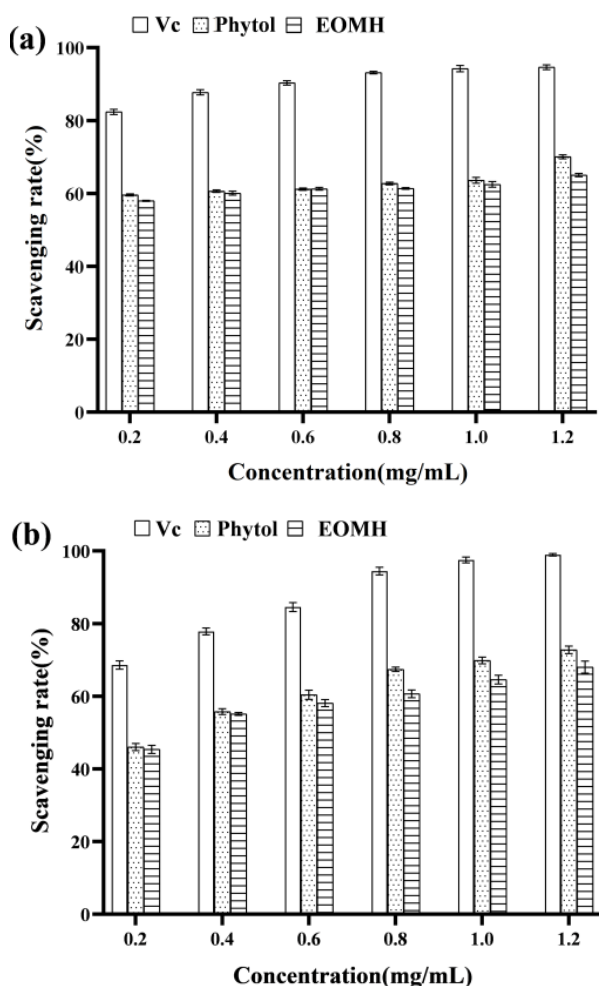
RI is the retention index determined by the database NIST 05; RI\* is the retention index calculated according to the retention time of C<sub>8</sub> - C<sub>40</sub> *n*-alkanes



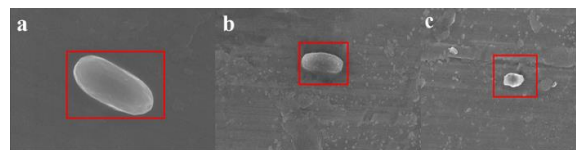
**Fig. 4:** Contours and 3D RSM images showing the effects of between-factor interactions on the extraction rate. Extraction time versus Particle size (a, b); Extraction time versus Liquid-to-solid ratio (c, d); Particle size versus Liquid-to-solid ratio (e, f)



**Fig. 5:** Infrared spectra of phytol and EOMH



**Fig. 6:** The in vitro antioxidant activities of EOMH and phytol using Vc as positive control. (a) DPPH<sup>•</sup> scavenging capabilities; (b) <sup>•</sup>OH scavenging capabilities. Data was shown as means ± SD (n = 3)



**Fig. 7:** SEM images of untreated *E. coli* suspension (a); *E. coli* suspension treated with phytol (b); *E. coli* suspension treated with EOMH (c)

## Discussion

In this investigation, the single-factor experiments for EOMH extraction were first conducted for obtaining the independent variables of RSM optimization. From Figs. 1 to 3, we can observe that extended extraction time and increased particle size as well as excessive liquid-to-solid ratio resulted in a sharp decline in EOMH extraction yield. These phenomena could be uncovered by the following explanations: (1) If the extraction time was too short, due to insufficient heating, the internal structures of materials were not fully destroyed, which largely decreased the release of targeting essential oil. When the materials were sufficiently heated, the release of targeting essential oil was promoted and EOMH yield was largely raised. However, when heating was excessive, the essential oil may flow back with steam, leading to partial consumption and decreasing the extraction rate (Zhang *et al.*, 2014b). (2) If the particle size of dried *M. hispida* was too low, due to the excessively large gaps between materials, heat from steam is easy to escape from the gaps, leading to insufficient heating and restricted the release of essential oil from materials. Generally, to decrease particle size of materials is beneficial for enlarging the surface area, facilitating the even penetrate of heat from steam in materials (Zheljazkov *et al.*, 2014). However, since the extraction was conducted in heterogeneous phase, the materials with too small particle size were apt to be highly dispersed in water, hindering the diffusion of steam, thereby lowering the extraction rate of EOMH (Kusuma and Mahfud, 2016). (3) At low liquid-to-solid ratio, the materials were excessive and cannot be evenly mixed with water (Pourmortazavi and Hajimirsadeghi, 2007). As the liquid-to-solid ratio increased, the materials was in full contact with water to weaken the mass transfer resistance during heating (Najafian, 2013), which can improve the extraction of essential oil. When the liquid-to-solid ratio increased further, the evaporated compounds were apt to be redissolved in the abundant water, which may decrease the yield of essential oil (Milojević *et al.*, 2008).

Then, to optimize EOMH extraction, a three-level-three-factor RSM was designed by BBD using EOMH extraction rate as response value. In previous work, we found that the non-optimized extraction rate of essential



oil from fresh *M. hispida* was 0.27% (Zheng *et al.*, 2019). In this study, considering prolonging the preservation time of *M. hispida* and facilitating the continuous industrial production, we took dried *M. hispida* as raw material to optimize the extraction process of essential oil. The results indicated that although drying may cause the loss of some low-boiling compounds, after process optimization, the loss can be remedied to some extent, making the extraction rate of essential oil from dried *M. hispida* reach 0.31%, which was still higher than that from fresh *M. hispida* (0.27%).

After that, GC-MS was applied to reveal the chemical profile of EOMH (Table 4). Compared with EOFMH (Zheng *et al.*, 2019), there were eight compounds missing in EOMH, considering that these volatile compounds were lost during the drying process of fresh *M. hispida* (Tang *et al.*, 2014). Amazingly, the content of phytol in EOMH was raised to 53.6%, which was 9.84% higher than that in EOFMH, suggesting that drying at 60°C could be a beneficial processing for the accumulation of phytol in EOMH. Due to the fact that phytol is a famous diterpenoid that possesses prominent bioactivities, particularly antibacterial capacity (Jeong, 2018; de Santos *et al.*, 2013), thus present process would provide a suitable way to obtain phytol-rich essential oil from dried *M. hispida*.

The chemical profile of EOMH was further confirmed by FT-IR analysis by using phytol as a control. The FT-IR spectrum comparison of EOMH and phytol (Fig. 5) suggested that EOMH appears to be dominated by phytol. This finding was highly consistent with that of GC-MS analysis (Table 4).

It is deduced from our previous work that the antioxidant ability of phytol may partially contribute to the inhibitory effect of EOMH against *E. coli* (Zheng *et al.*, 2019). Thus, in present work, the antioxidant abilities of EOMH and phytol were further compared.

Hydroxyl radical is the most active reactive oxygen species. It can react with almost any molecules in living cells (Hou *et al.*, 2020). While, DPPH radical (DPPH<sup>•</sup>) is a very stable nitrogen-containing free radical. If the tested substance can quench DPPH<sup>•</sup>, which may indicate that the tested substance possesses high scavenging capacities against other unstable radicals such as hydroxyl, alkyl and peroxide free radicals (Zheng *et al.*, 2015). Therefore, in this study, the antioxidant potentials of EOMH were assessed using these two radical models.

As shown in Fig. 6, EOMH possessed similar scavenging capacities against DPPH and hydroxyl radicals with those of phytol, indicating that the antioxidant ability of EOMH could be mainly contributed by phytol.

Finally, the preliminary inhibitory mechanism of EOMH on *E. coli* was further disclosed via SEM observation. As shown in Fig. 7, these changes on *E. coli* surface morphology revealed that EOMH would elicit little higher antibacterial capacities against *E. coli* than that of phytol, suggesting that other factors in addition to the antioxidant mechanism would affect the inhibitory effects of EOMH against *E. coli*. Reportedly, the esters and alkanes of essential oils can collaboratively exert bacteriostatic effects via degrading and destroying the cell walls and membranes of *E. coli*, leading to intracellular leakage even cell death (Zhan *et al.*, 2014a). Further research is undergoing.

## Conclusion

Based on preliminary results obtained from our previous work (Zheng *et al.*, 2019), the extraction optimization, constituent identification, *in vitro* antioxidant capacity measurement and preliminary inhibitory mechanism against *E. coli* of *Essential oil* from dried *M. hispida* (EOMH) were conducted. On the basis of single-factor tests, EOMH extraction was optimized by RSM and BBD to give the optimal conditions: Extraction time of 7 h, particle size of 20 mesh and liquid-to-solid ratio of 30: 1 (mL/g), under which the highest extraction rate was found to be 0.31%. Nineteen components were identified in EOMH by GC-MS and phytol content accounted for 53.6%, which was 9.84% higher than that in the *Essential oil* from Fresh *M. hispida* (EOFMH) (Zheng *et al.*, 2019). Infrared spectroscopy showed that EOMH has characteristic absorption peaks similar to those of phytol, which further validated the results that EOMH is dominated by phytol (Table 4). Antioxidant evaluation showed that the antioxidant ability of EOMH could be mainly contributed by the relatively higher proportion of phytol. SEM analysis demonstrated that EOMH is more destructive to *E. coli* than that of phytol. It was deduced that other factors would equally affect the inhibitory effects of EOMH against *E. coli* besides the antioxidant mechanism. Hence, two issues are planned to be further studied in the future: (1) To further explain the antibacterial mechanism of EOMH against *Escherichia coli* by Transmission Electron Microscopy (TEM), cell membrane permeability measurement and the effects on the physiological metabolism; (2) To develop novel EOMH-based antioxidants and bacteriostatic agents by using *M. hispida* as raw materials.

Finally, this study is expected to offer a scientific basis for high-valued utilization of *M. hispida* species.

## Funding Information

This work was supported by the innovation training program and the key graduation thesis program for undergraduate students of Changshu Institute of Technology.

## Author's Contributions

**Xiulan Chu and Tong Wang:** Performed the experiments of extraction and antioxidant capacity.

**Qianfeng Chen, Xinyu Bai and Chen Pan:** Carried out FT-IR analysis and bacteriostatic experiments.

**Yang Zhang:** Designed the experiments, revised the manuscript and polish the manuscript.

**Lixue Zheng:** Designed the experiments, wrote the manuscript and polish the language.

## Ethics

This article is original and contains unpublished material. The corresponding author confirms that all of the other authors have read and approved the manuscript and no ethical issues involved.

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